



Targa Sound Terminal

2628 Marine View Drive,
Tacoma, WA 98422
Tele. (253) 272-9348 1-800-426-9799
Fax (253) 272-5686

December 21, 2011

Mr. Gerry Pade
Air Pollution Engineer
Puget Sound Clean Air Agency
1904 3rd Ave Ste. 105
Seattle, WA 98101

RE: Targa Sound Terminal Renewable Fuels Expansion Project follow up:

Dear Mr. Pade,

In response to your Notice of Construction Worksheet for NOC 10325, additional considerations were made to focus on an aggregate emission increases for multiple aspects of gasoline loading including tank losses, component losses, and truck loading / fugitive losses.

URS Corp. was hired by Targa Sound Terminal (previously known as Sound Refining, Inc.) to provide expertise and consultation for the purpose of addressing acceptable source impact levels (ASIL) pertaining to gasoline loading. This included running EPA TANKS 4.09d for any effected tank, calculating TAC emissions for ASIL consideration based on loading and working losses, preparation of a wind rose model based on local meteorological data, and mapping of TAC level impacts.

URS calculated throughput data using the maximum gasoline throughput for the existing VRU of 501,875,000 gal/yr (32738 bbl/day). For this process, four new tanks have been submitted for agency approval, these tanks are designated as 201, 202, 203, and 204 and would hold the majority of gasoline at the facility. However to be flexible Targa Sound Terminal has modeled all tanks with internal floating roofs at the facility for possible gasoline storage, this includes tanks 150, 152, 153, 154, 155, and 156.

The findings of the aggregate model created by URS show that all TAC values are below their ASIL limits.

After researching potential gasoline suppliers, including companies such as Conoco Philips a 1,3 Butadiene speciation value was asked for. The refiners informed Targa Sound Terminal that Butadiene levels in the existing gasoline provided were considered

to be at non-detectable levels. As such, Targa Sound Terminal does not believe that 1,3 Butadiene should be a limiting factor for gasoline throughput.

For the purposes of loading crude oil over the Targa Sound Terminal Marine dock, the facility had estimated vessel fugitive leak values using the SCAQMD method for leak estimates, however to clarify all values these figures were recalculated using the EPA *Protocol for Equipment Leak Emission Estimates* (table 2-3).

Targa Sound Terminal's requests for this current permit package include:

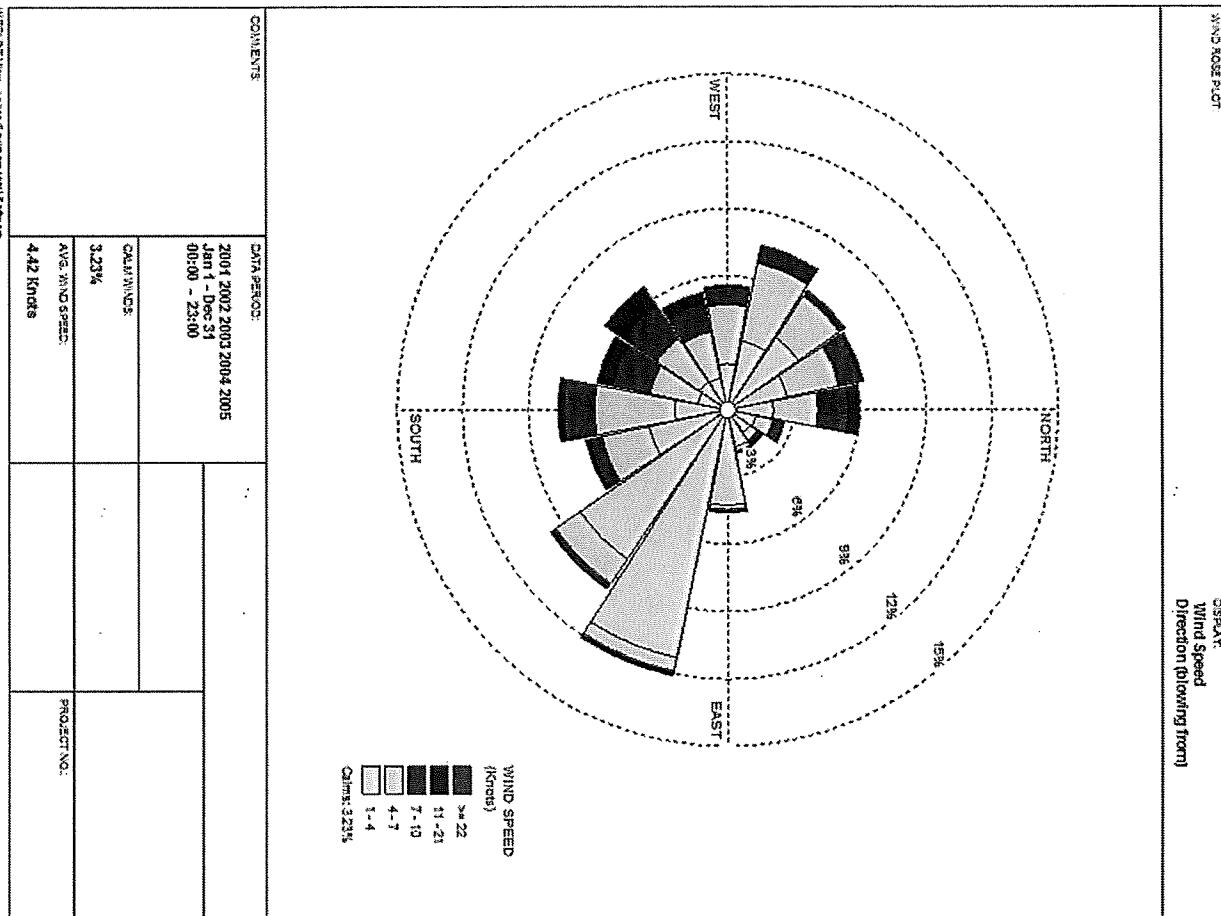
- 1.) Adjustment of the instantaneous rate of the existing VRU to be increased from 2,400 gpm to 3,600 gpm based on previously submitted documentation from the John Zink Company.
- 2.) Permitting of the new Vapor Recovery unit as per the previously submitted documentation that additionally will allow for marine loading of gasoline, crude, and ethanol.
- 3.) That the maximum combined loading throughput should not exceed the total VRU(s) capacity.
- 4.) The terminal should not exceed 100 tons VOC per year.
- 5.) Targa Sound Terminal is requesting an annual gasoline throughput of 501,875,000 gallons based on the benzene acceptable source impact level.
- 6.) Targa Sound Terminal has requested that the floating roof tanks at the terminal be permitted for gasoline, crude, and other fuel oils service. The tanks that this request pertains to are tanks 150, 151, 152, 153, 154, 155, 156, 157, 162, 201, 202, 203, and 204.
- 7.) The terminal has requested additional load arms to be installed at the bottom loading truck rack. The request is to bring each load spot at lanes 3, 4, and 5 up to four arms per load spot (two load spots per lane) for a total of 24 arms. Of those 24 load arms, 10 have already been permitted and installed.

Attached with this letter are the following documents

- 1.) Wind rose model.
- 2.) Benzene dispersion map
- 3.) Component Fugitive leak emission calculations, (total including marine)
- 4.) AERMOD TAC Summary of Results
- 5.) AERMOD Source Inputs (3)
- 6.) Permit package for tanks 201, 202, 203, and 204.

Thank you for your attention on this matter.

Matthew Kolata
Targa Resources



URS

Figure 1: Location of the Maximum Annual Benzene Concentration (ug/m³)



AERMOD Summary of Results

Toxic Air Pollutant	CAS #	Averaging Period	ASIL (ug/m ³)	Maximum Off-Site Concentration (ug/m ³)		
				2003	2004	2005
Ethylbenzene	100414	year	0.4	0.040	0.041	0.025
M & p-xylene	108383; 106423	24-hr	221	0.573	0.654	0.479
Toluene	108883	24-hr	500	1.030	1.186	0.862
N-hexane	110543	24-hr	700	0.505	0.520	0.422
Cyclohexane	110827	24-hr	6000	0.059	0.061	0.05
Benzene	71432	year	0.0345	0.013	0.012	0.008
O-xylene	95476	24-hr	221	0.213	0.219	0.177
Isopropylbenzene (cumene)	98828	24-hr	400	0.009	0.010	0.008
1,3- Butadiene	106990	year	0.00588	0.000	0.000	0.000

maximum values

AERMOD Point Source Inputs

POINT	1yr=	8760 hrs	CAS	ANNUAL		26		24		24		ANNUAL		26		24		
				108-38-3	105-42-3	108-38-3	110-54-3	110-82-7	71-43-2	95-47-6	98-82-3	98-82-3	Isopropylbenzene	(cumene)	1,3-Butadiene		ANNUAL	
Source ID				Ethylbenzene	M & propylene	Toluene	N-hexane	Cyclohexane	Benzene	O-xylene								105990
VRU	VRU	3464105	5236190	1.25	6.096	0	9.57	0.1524	2.10051E-06	7.50035E-06	1.38701E-05	6.81073E-06	7.95645E-07	6.42624E-07	2.86433E-06	1.27393E-07	2.30742E-09	

AERMOD Area Source Inputs

AREA

AERMOD Area Circle Source Inputs (Tanks)

Area Circ	1yr=	8760 hrs	ANNUAL		24	24	24	24	ANNUAL	ANNUAL	24	ANNUAL	
			100-41-4	42-3	108-38-3; 106-	108-88-3	110-54-3	110-82-7	71-43-2	95-47-6	98-82-8	Isopropylbenzene	
			Ethylbenzene	M & p-xylene	Toluene	N-hexane	Cyclohexane	Benzene	Oxyylene	1,3-Diisobutylbenzene	1,3-Isopropylbenzene (cumene)	106990	
Source ID	Source Desc.		Easting (X) (m)	Northing (Y) (m)	Base Elevation (m)	Release Height (m)	Radius of Circle (m)	Number of Vertices	Vertical Dimension (m)	10414 (lb/hr)	106423 (lb/hr)	10883 (lb/hr)	110543 (lb/hr)
TK152	TANK 152	546393.8	523621.8	18.288	13.11	0.000159438	0.00052094	0.001059	0.000501577	5.85209E-05	4.95E-05	0.000211	9.36335E-06
TK155	TANK 155	546363	523621.2	15.24	9.27	0.00033899	0.001591223	0.002219	0.001045145	0.000121915	0.000104	0.000439	1.95064E-05
TK156	TANK 156	546363.4	523618.6	15.24	9.19	0.000157059	0.000691958	0.001047	0.000443382	5.64054E-05	4.93E-05	0.000203	9.02486E-06
TK150	TANK 150	546367.2	523612.9	12.192	6.4	0.000177471	0.000771987	0.001182	0.000548808	6.39342E-05	5.61E-05	0.00023	1.02375E-05
TK153	TANK 153	546386.7	5236065	10.668	7.32	0.00019111	0.000792997	0.00127	0.000598876	6.98615E-05	5.93E-05	0.000252	1.11778E-05
TK154	TANK 154	546405.6	5236060	10.668	7.62	0.00019111	0.000792997	0.00127	0.000598876	6.98615E-05	5.96E-05	0.000252	1.11778E-05
	TANK 201	546278.9	5236318	17.0688	17.0688	0.0001913153	0.000627933	0.0126327	0.000623256	0.000724679	0.000649	0.0002509	0.000115949
	TANK 202	546273.2	5236347	17.0688	17.0688	0.001818097	0.0006583315	0.01201	0.005895041	0.0006588673	0.000617	0.002479	0.000110188
	TANK 203	546247.8	5236331	17.0688	17.0688	0.001818097	0.0006583315	0.01201	0.005895041	0.0006588673	0.000617	0.002479	0.000110188
	TANK 204	546219.5	5236338	17.0688	17.0688	0.001818097	0.0006583315	0.01201	0.005895041	0.0006588673	0.000617	0.002479	0.000110188

Throughput	Benzene	1,3-Butadiene
Annual Emissions (t/year) @ 1,344,031 gallons/day	8.18 1.18E-04	1.41 2.02E-05

Conversions

0.002	mg benzene/liter fuel*	0.0003	mg 1,3 butadiene/liter fuel
1000	mg/g	1000	mg/g
453.59	g/lb	453.59	g/lb
3.78	l/gal	3.78	l/gal
1,344,031.30	gal/day	1,344,031.30	gal/day
365	day/yr	365	day/yr
8.176	lbs benzene/year	1,405	lbs 1,3 butadiene/year
490,571,424.00	gal/year	490,571,424.00	gal/year
5.82	Benzene/Butadiene Ratio ¹		

* John Zink emission rate
1,Conoco Phillips TAC weight % ratio

100-41-4	108-38-3; 106-42-3	108-88-3	110-54-3	110-82-7	71-43-2	95-47-6	98-82-8	10690
Ethylbenzene	M & p-xylene	Toluene	N-hexane	Cyclohexane	Benzene	Isopropylbenzene (cumene)	1,3-Butadiene	
Degassing								
John Zink 99% Control Efficiency								
Total VRU + Degassing (lb/yr)	0.01840043	0.066631861	0.121554	0.059562001	0.00696986	0.005512	0.025091	0.00115178
	0.01840043	0.066631861	0.121554	0.059562001	0.00696986	5.63E-03	0.025091	2.02E-05



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General:

Targa Sound Terminal will construct four new tanks within the facility. Three of the tanks will have an 80' diameter with a working capacity of 50,135 barrels each, and the fourth tank will have a 95' diameter with a working capacity of 70,698 barrels. These tanks will contain internal floating roofs, and will provide additional storage for the expansion of the facility. The tanks have been designated as 201 (95'), 202, 203, and 204 (80').

To reduce emissions, the floating legs for the roof will be removable and capped/sealed while the tanks are in service.

General Information (Tank 201)

1. Type of construction:	New
2. Date of construction:	2012
3. Hours of operation:	24/7
4. Estimated installation start date:	

Liquid Properties (Tank 201)

1. Products stored:	Gasoline
	Distillates
	Crude
2. Maximum Storage Temp.	Ambient
3. Vapor pressure at max storage temp	5 – 15 RVP
4. Estimated annual throughput(gal/yr)	142,527,168

Design of Internal Floating Roof Tank (201)

1. Working diameter	95'
2. Working capacity (gal)	2,969,310
3. External shell color/shade	White
4. External shell condition	Good
5. Roof color/shade	White
6. Roof paint condition	Good
7. Number of columns supporting fixed roof	(1) Double channel support column
8. Effective column diameter	2.75" x 12"
9. Type of primary seal	Mechanical shoe
10. Type of secondary seal	Mechanical rim seal
11. Type of deck	Steel, welded
12. Number of each type of deck fitting	
a. 24" Manway	1
b. 19" float well	1
c. 10" vacuum breaker	1
d. 4" gauge/guide pole	1
e. 18" x 30" ladder well	1
f. 3" emergency roof drain	1

Operation and Maintenance (Tank 201)

1. Method used to fill tank	Truck, railcar, barge, pipeline
2. Method used to drain tank	Truck, barge
3. Describe preventative maintenance	Tank 201 will be inspected and maintained to API 653 standards

General Information (Tank 202)

5. Type of construction:	New
6. Date of construction:	2012
7. Hours of operation:	24/7
8. Estimated installation start date:	

Liquid Properties (Tank 202)

5. Products stored:	Gasoline
	Distillates
	Crude
6. Maximum Storage Temp.	Ambient
7. Vapor pressure at max storage temp	5 – 15 RVP
8. Estimated annual throughput(gal/yr)	101,071,728

Design of Internal Floating Roof Tank (202)

13. Working diameter	80'
14. Working capacity (gal)	2,105,661
15. External shell color/shade	White
16. External shell condition	Good
17. Roof color/shade	White
18. Roof paint condition	Good
19. Number of columns supporting fixed roof	(1) Double channel support column
20. Effective column diameter	2.75" x 12"
21. Type of primary seal	Mechanical shoe
22. Type of secondary seal	Mechanical rim seal
23. Type of deck	Steel, welded
24. Number of each type of deck fitting	
a. 24" Manway	1
b. 19" float well	1
c. 10" vacuum breaker	1
d. 4" gauge/guide pole	1
e. 18" x 30" ladder well	1
f. 3" emergency roof drain	1

Operation and Maintenance (Tank 202)

4. Method used to fill tank	Truck, railcar, barge, pipeline
5. Method used to drain tank	Truck, barge
6. Describe preventative maintenance	Tank 202 will be inspected and maintained to API 653 standards

General Information (Tank 203)

9. Type of construction:	New
10. Date of construction:	2012
11. Hours of operation:	24/7
12. Estimated installation start date:	

Liquid Properties (Tank 203)

9. Products stored:	Gasoline
	Distillates
	Crude
10. Maximum Storage Temp.	Ambient
11. Vapor pressure at max storage temp	5 – 15 RVP
12. Estimated annual throughput(gal/yr)	101,071,728

Design of Internal Floating Roof Tank (203)

25. Working diameter	80'
26. Working capacity (gal)	2,105,661
27. External shell color/shade	White
28. External shell condition	Good
29. Roof color/shade	White
30. Roof paint condition	Good
31. Number of columns supporting fixed roof	(1) Double channel support column
32. Effective column diameter	2.75" x 12"
33. Type of primary seal	Mechanical shoe
34. Type of secondary seal	Mechanical rim seal
35. Type of deck	Steel, welded
36. Number of each type of deck fitting	
a. 24" Manway	1
b. 19" float well	1
c. 10" vacuum breaker	1
d. 4" gauge/guide pole	1
e. 18" x 30" ladder well	1
f. 3" emergency roof drain	1

Operation and Maintenance (Tank 203)

7. Method used to fill tank	Truck, railcar, barge, pipeline
8. Method used to drain tank	Truck, barge
9. Describe preventative maintenance	Tank 203 will be inspected and maintained to API 653 standards

General Information (Tank 204)

13. Type of construction:	New
14. Date of construction:	2012
15. Hours of operation:	24/7
16. Estimated installation start date:	

Liquid Properties (Tank 204)

13. Products stored:	Gasoline
14. Maximum Storage Temp.	Distillates
15. Vapor pressure at max storage temp	Crude
16. Estimated annual throughput(gal/yr)	Ambient
	5 – 15 RVP
	101,071,728

Design of Internal Floating Roof Tank (204)

37. Working diameter	80'
38. Working capacity (gal)	2,105,661
39. External shell color/shade	White
40. External shell condition	Good
41. Roof color/shade	White
42. Roof paint condition	Good
43. Number of columns supporting fixed roof	(1) Double channel support column
44. Effective column diameter	2.75" x 12"
45. Type of primary seal	Mechanical shoe
46. Type of secondary seal	Mechanical rim seal
47. Type of deck	Steel, welded
48. Number of each type of deck fitting	
a. 24" Manway	1
b. 19" float well	1
c. 10" vacuum breaker	1
d. 4" gauge/guide pole	1
e. 18" x 30" ladder well	1
f. 3" emergency roof drain	1

Operation and Maintenance (Tank 204)

10. Method used to fill tank	Truck, railcar, barge, pipeline
11. Method used to drain tank	Truck, barge
12. Describe preventative maintenance	Tank 204 will be inspected and maintained to API 653 standards